



Development of a modular eightchamber Multifunctional Anaerobic Baffled Reactor

6th Biorefinery Day: Key technologies for bio-based products and fuels

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Why Anaerobic Baffled Reactor?

Resilient and stable:

Compartmentalised design tolerates shocks and feed variability better than conventional ADs.

• Efficient design:

Simple, low-maintenance, cost-effective setup that improves methane quality and recovery.

Biomass retention:

Staged chambers specialise microbes, reduce sludge, and boost robustness.

Beyond biogas:

Enables high-value products and chemicals, supporting circular bio-economies.

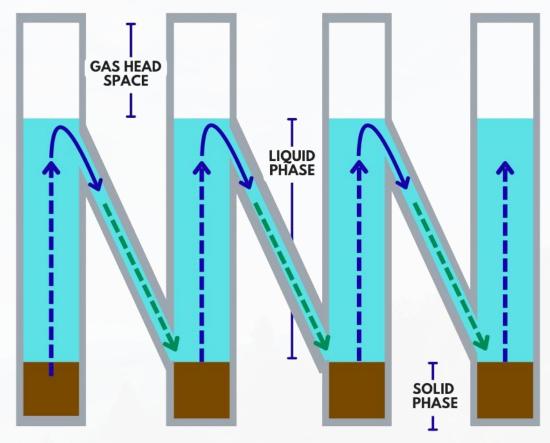


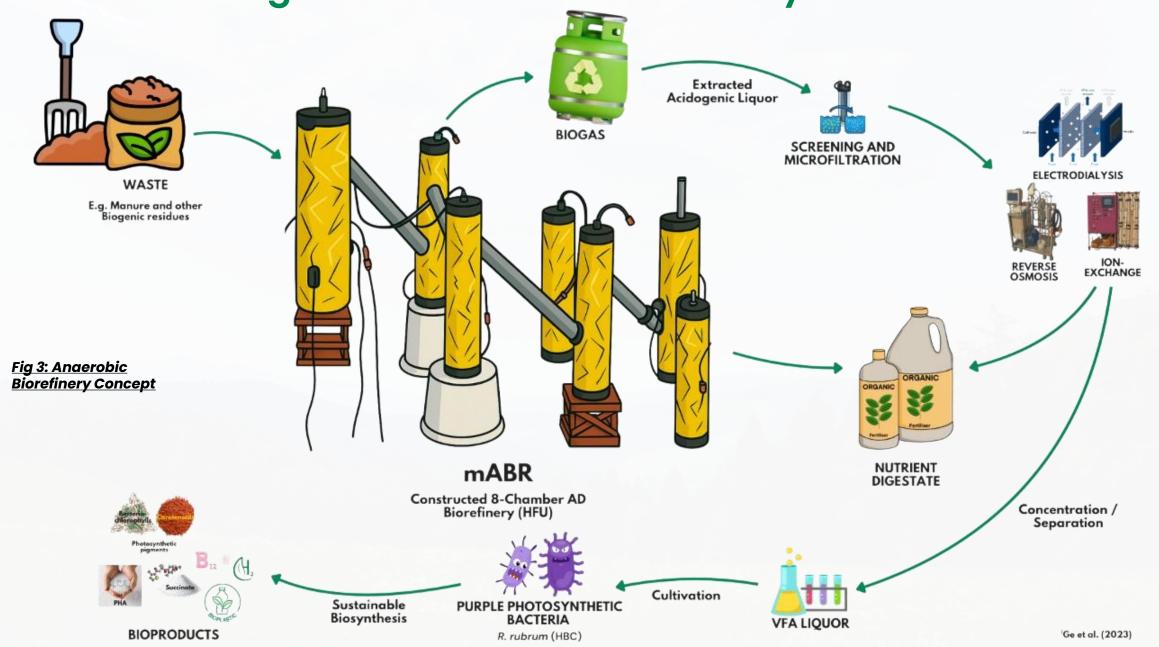
Fig 1: Modular Anaerobic Baffled Reactor with separated chambers



Fig 2: Anaerobic Digestion Stages

mABR: The Engine of a Circular Biorefinery







Our Design: 8-Chamber ABR ≈ 17 L

PVC/PP Tube Frame

Chamber No. 1, 7, 8: Ø 110 mm, H 420 mm **≈ 3.25 L** Chamber No. 2-6: Ø 75 mm, H 440 mm **≈ 1.4 L**

Heating

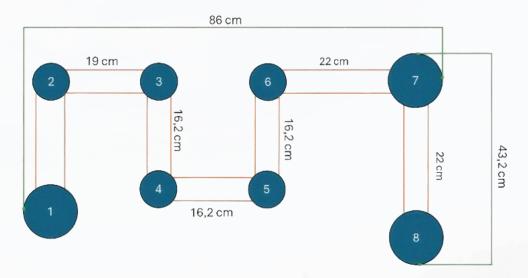
Electric 14 W and 20 W heating pads (each chamber)

Sensing:

DS18B20 temperature sensors and Webcam connected to Raspberry Pi microcontroller

Sampling:

Liquid/Solids: Metal Valves and internal tubes. Gas: Biogas collection bags.



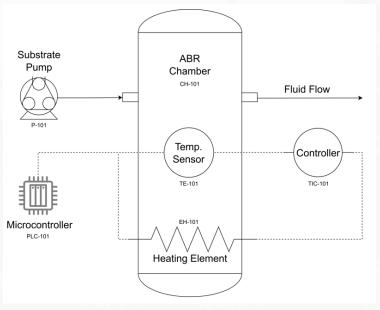


Fig 4: (a) Plan view of ABR layout, (b) Simplified P&ID Diagram



Unique Features of our ABR

- Low-cost Construction (PVC/PP):
 Standard fittings, durable; markedly lower capex (≈ 800€) than glass/steel.
- Modular 8-chamber series (17 L):
 Isolated stages for sampling/control; less short-circuiting.
- Zoned thermal control:
 Per-chamber heating pads enable
 setpoint gradients and energy efficiency
 (~0.4 kWh/L/day)
- Online temperature:
 DS18B20 sensors for continuous profiles and tighter process control.

Intermediate scale:

17 L bridges bench- to pilot-scale, improving hydrodynamics, sampling and data relevance.



Fig 5: Assembled 17 L 8-Chamber ABR



Mesophilic-thermophilic phase anaerobic co-digestion Trial

- Stable, VFA-rich intermediates, while elevating methanogenesis (≈ 45.0 °C) accelerates kinetics without instability of full thermophilic digestion
- 46 °C → 44 °C: Lower free NH₃ toxicity; methanogen niches; residual VFA polishing

Set points:

- Flow: 6.94 mL/ min ≈ HRT 1.7 days
- Temperature:

Chamber 1 (preheat 42 °C)

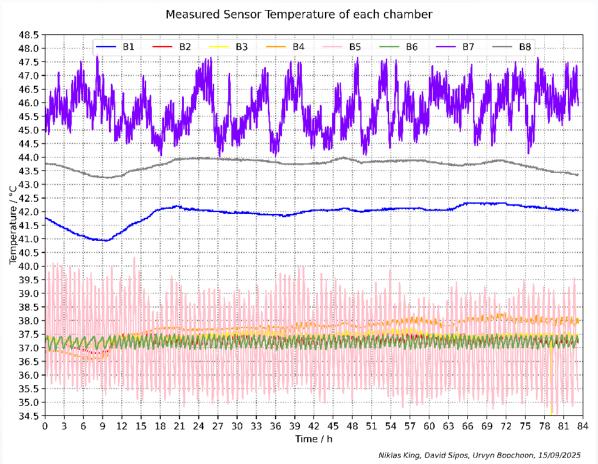
Chamber 2-6: 37.0 °C

Chamber 7: 46.0 °C

Chamber 8: 44.0 °C

Initial Findings:

 Settles around targets; but, additional heating pads caused fluctuations in later Chambers



<u>Fig 6: Results of preheated operation using water as substrate; B1 - B8</u> (Chamber 1 - 8)



Temperature results

Attained Temperature averages

Chamber 1 (preheat)

Chamber 2-6 ≈ 37.35 °C

Chamber 7 ≈ 45.77 °C

Chamber 8 ≈ 43.73 °C

Temperature zones

Mean confirms temperature gradient between the mesophilic (Chamber 2-6) and (low) thermophilic chambers (Chamber 7-8)

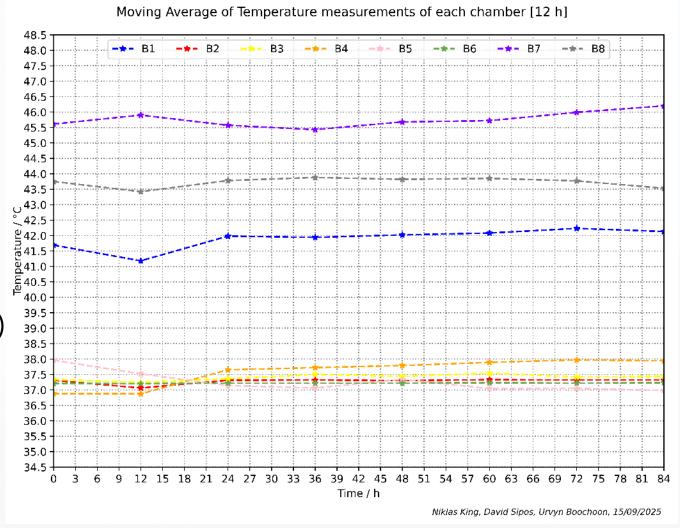


Fig 7: Moving average results every 12 hours of preheated operation using water as substrate; B1 - B8 (Chamber 1 - 8)



Temperature Control – Problems & Solutions

Problems

- Large fluctuations (±1−2 °C)
- Uneven heating from concentrated pads
- Insufficient heat (preheating)
- Ambient losses due to insulation

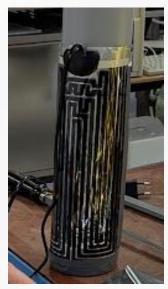
Solutions

- Add more, lower-power pads for smoother heating
- Improve insulation (bubble foil / wrap)
- Optimise pad placement for even coverage
- Use Pi-relay control with tighter switching thresholds
- Position sensors away from direct pad contact









<u>Fig 8: Heating pad, insulation, sample points</u> and sensors



Next Stage - Anaerobic Digestion Experiments

Baseline:

Starch/manure feed, 37 °C all chambers

Zoning trials:

Heat zones (44-46 °C in Ch. 7-8, later 1-2 & 7-8)

Monitoring:

COD/VFAs, CH₄ yield, 16S microbiology, energy balance

Outcomes:

Rate effect of warm zones, energy trade-off, operating rules

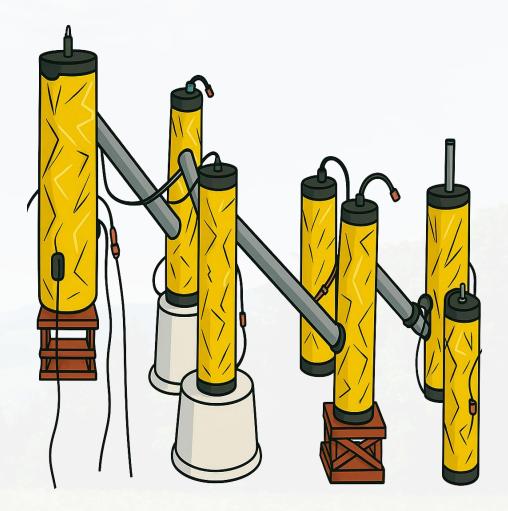


Fig 9: mABR concept

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PROJECT







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